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PATENT APPLICATION

Attorney Docket No. P96107US (38222/1P)

TITLE OF THE INVENTION

Fluid Filter Using Floating Media

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CROSS-REFERENCE TO RELATED APPLICATIONS

10 This is a continuation-in-part application of co-
pending U.S. patent application Serial No. 08/179,452,
filed January 10, 1994, now U.S. Patent No. 5,573,663,
both incorporated herein by reference.

STATEMENT REGARDING FEDERALLY SPONSORED RESEARCH OR DEVELOPMENT

15 Not applicable

REFERENCE TO A "MICROFICHE APPENDIX"

Not applicable

BACKGROUND OF THE INVENTION

1. Field of the Invention

20 The present invention relates to filters for fluids.
More particularly, the present invention relates to a
filter system for fluids which utilizes filter media having
a density different from the fluid (such as buoyant plastic
beads when water is being filtered).

25 2. General Background of the Invention

In the filtration of fluids, filter media in the form
of plastic beads or other particulates, such as
diatomaceous earth or sand, is used to trap impurities.
Typically, the filter media must be backwashed at
30 predetermined intervals to keep the filter operating
smoothly. This backwashing requires that the filter system
be shut down, which can be quite inconvenient if continuous
filtration is required during processing. If that is the
case, then the process must be shut down while the filter
35 is being backwashed, resulting in undesirable loss of
production.

U.S. Patent No. 5,126,042 discloses such a filter. In

addition to the problem of needing to shut the system down to backwash the filter, static filters such as the one disclosed in the '042 patent can suffer from tunneling problems. Tunneling occurs when the filter media get
5 clogged or bacterial gel builds up on the media, causing the filter media to stick together. Water breaks tunnels through the filter media and, following the path of least resistance, continues to travel through the tunnels instead of getting filtered by the filter media.

10 BRIEF SUMMARY OF THE INVENTION

The apparatus of the present invention is a filter system in which backwashing is not necessary, as the filter media is constantly rejuvenated. The apparatus of the present invention comprises a tank means for containing a
15 volume of fluid, an influent means for introducing the fluid into the tank means, an effluent means for allowing filtered fluid to exit the tank means, and filter media for filtering predetermined matter (such as particulates, which may be impurities) out of the fluid. In the tank means
20 there is a filter zone where the filter media is relatively tightly packed, a mixing zone where the filter media is relatively loosely packed, and a quiet zone adjacent the mixing zone, the mixing zone being between the filter zone and the quiet zone. An important feature of the present
25 invention is a conveyer means for conveying filter media from the filter zone to the quiet zone.

Preferably, the filter zone is adjacent the effluent means, the mixing zone is between the influent means and the filter zone, and the quiet zone is below the mixing
30 zone.

When the fluid being filtered is water, the filter media preferably comprises buoyant beads and the conveyer means can comprise a screw auger. When the fluid is water, the predetermined matter usually comprises solid
35 impurities. There is a motor means for turning the screw auger and a duct means for containing the screw auger. The influent means preferably includes pipes which secure the

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duct means to the wall of the tank means. There is a waste outlet for extracting predetermined matter from the quiet zone.

5 The conveyer means can be water-powered, as described in the detailed description of the invention, so that the number of moving parts of the invention is reduced. However, the water-powered version ties together the flow rate of water through the filter to the flow rate of beads through the conveyer means.

10 The effluent means can comprise a plurality of effluent pipes and means for stopping fluid flow out of the tank means through at least one effluent pipe while fluid flows out of the tank means through at least one other effluent pipe.

15 The filter apparatus can be a part of a system comprising, in addition to the apparatus mentioned above, a fish tank containing live fish and water, the water in the fish tank being the fluid being filtered in the tank means, and the filter media being buoyant in the water.
20 There is preferably also a pump for pumping water from the fish tank to the tank means. In such a case, most of the predetermined matter being filtered would be particulates denser than water.

25 The method of filtering fluid of the present invention comprises the steps of providing a tank means for containing a volume of fluid, introducing the fluid into the tank means, providing a filter media for filtering predetermined matter out of the fluid, causing the filter media to pack relatively tightly in a filter zone in the
30 tank means, flowing the fluid through the filter zone where predetermined matter in the fluid become trapped in the filter media, flowing the filtered fluid out of the tank means, conveying the filter media and trapped predetermined matter from the filter zone to a quiet zone where the
35 predetermined matter moves away from the filter zone and the filter media move in the direction of the filter zone, and allowing the filter media to move from the quiet zone

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Preferably, the filter media and trapped predetermined matter are continuously conveyed from the filter zone to the quiet zone. Usually, when the fluid being filtered is water, the trapped predetermined matter comprises particulates which drop to the bottom of the tank means in the quiet zone.

10 For a further understanding of the nature, objects,
and advantages of the present invention, reference should
be had to the following detailed description, read in
conjunction with the following drawings, wherein like
reference numerals denote like elements and wherein:

Figure 2 shows a fish tank system in which the filter apparatus of the present invention is being used.

Figure 4 is a sectional view of the second embodiment of the apparatus of the present invention.

Figure 6 is a sectional view of a fourth embodiment of the apparatus of the present invention.

Figure 8 is a sectional view of the preferred embodiment of the apparatus of the present invention.

35 Figure 10 is an exposed view of internal components of
the embodiment of Figure 9.

Figure 11 is a top view of the embodiment of Figure 9.

Figure 12 is a typical in-tank installation for growing fish or other aquatic species of the filter apparatus of the present invention.

Figure 13 is a cut-away view of the filter shown in Figure 12.

Figures 14, 15, 16 and 17 show hydraulic apparatus which creates the preferably 360 degree vertical/elliptical cycling of filter media in the hydraulically driven filter apparatus of the present invention.

10 PARTS LIST

The following is a list of suitable parts and materials for the various elements of the preferred embodiment of the present invention.

- 10 filter apparatus of a first embodiment of the present
- 15 invention
- 11 buoyant filter media (preferably polypropylene or polyethylene)
- 15 quiet zone in tank 30
- 16 particulates to be filtered out of fluid 21
- 20 18 mixing zone where particulates 16 and the filter media 11 mix
- 19 filter zone where particulates 16 become trapped in the filter media 11
- 21 fluid (e.g., water) to be filtered
- 25 22 effluent pipes (could be screen pipe with a closed bottom)
- 23 filter area of effluent pipes
- 24 pump
- 25 influent pipe
- 30 26 influent ring
- 27 exit holes in influent ring 26
- 30 tank
- 31 cylindrical wall of tank 30 (stainless steel or fiberglass, e.g.)
- 35 32 conical bottom of tank 30
- 33 waste outlet of tank 30
- 34 valve for waste outlet 33

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- 35 conical top of tank 30 (filter media control cap)
40 conveyer means
41 auger, preferably 6" or 9" diameter Helicoid Conveyer Screw
5 42 counter-direction friction duct containing auger 41
(suitable means, not shown, secure it within tank 30)
43 exit holes in the bottom of duct 42
44 entrance of duct 42
45 motor for turning auger 41 (preferably variable-speed)
10 46 closed bottom of duct 42
47 flighting of auger 41
48 shaft of auger 41
50 fish tank
110 filter apparatus of the second embodiment of the
15 present invention
115 quiet zone in tank 130
118 mixing zone where particulates 16 and the filter media
11 mix
119 filter zone where particulates 16 become trapped in
20 the filter media 11
122 outer effluent pipes
123 filter area of inner pipes 124
124 inner strainer slide pipe
125 influent pipes (schedule 40 PVC or stainless steel)
25 127 exit holes in influent pipes 125
128 nozzles in exit holes 127 in influent pipes 125
130 tank
131 cylindrical wall of tank 130 (stainless steel or
fiberglass, e.g.)
30 132 conical bottom of tank 130
133 waste outlet of tank 130
134 valve for waste outlet 133
135 dome-shaped top of tank 130 (filter media control cap)
137 nylon bearing plate
35 138 stuffing box plate
139 threaded fittings for securing pipes 125 to tank 130
140 conveyer means

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- 141 auger, preferably 6", 9", or 12" diameter 1/2 pitch
Interlox Conveyer Screw
- 142 counter-direction friction duct containing auger 141
- 143 exit vents in the bottom of duct 142
- 5 144 entrance vents in duct 142
- 146 closed bottom of duct 142 (closed with bearing plate
137)
- 147 flighting of auger 141
- 148 shaft of auger 141
- 10 149 threaded fittings for securing pipes 125 to duct 142
- 151 ball float valve
- 152 ball retainer cage
- 153 ball of ball float valve 151
- 160 blades in quiet zone 130
- 15 210 filter apparatus of the third embodiment of the
present invention
- 230 tank (stainless steel or fiberglass, e.g.)
- 231 end wall of tank 230
- 232 V-shaped bottom of tank 230
- 20 233 curved top of tank 230
- 234 side wall of tank 230
- 235 compartment of tank 230
- 310 filter apparatus of the fourth embodiment of the
present invention
- 25 330 tank
- 335 compartment of tank 330
- 350 partition in tank 330
- 410 filter apparatus of the preferred embodiment of the
present invention
- 30 415 quiet zone of tank 430
- 418 mixing zone of tank 430
- 419 filter zone of tank 430
- 422 effluent pipes
- 425 influent pipes
- 35 426 influent direction-altering pipes
- 427 funnel
- 428 exit troughs

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- 429 exit screens
430 tank of apparatus 410 (stainless steel or fiberglass,
e.g.)
431 cylindrical wall of tank 430
5 432 flat bottom of tank 430
435 open top of tank 430
440 conveyer means
442 counter-direction friction duct
443 exit vents in the bottom of duct 442
10 445 deflector cone
510 reactor
515 settling zone
518 mixing zone
522 pipes
15 526 inlet nozzle
527 flange
528 multi-directional effluent distribution unit (MEDU)
529 media screen
530 reactor vessel
20 531 outer walls
535 top of the reactor vessel 530
539 supplemental inlets
542 down tube
544 V-notches
25 570 solids capturing media
585 drain port
590 screen frame
592 influent centering lock collar

DETAILED DESCRIPTION OF THE INVENTION

30 Figure 1 shows a first embodiment of the present invention, filter apparatus 10.

Filter apparatus 10 includes a tank 30 having a cylindrical wall 31, a conical bottom 32, and a conical top 35 (which can be considered a filter media control cap, as
35 will be described further). Tank 30 has a waste outlet 33 at the bottom thereof. There is a valve 34 for controlling flow out of waste outlet 33.

In tank 30 there is a fluid 21 (e.g., water) to be filtered and a buoyant filter media 11 (preferably polypropylene or polyethylene) with which to filter the fluid.

5 Tank 30 includes a mixing zone 18 where particulates 16 and the filter media 11 mix, a filter zone 19 where particulates 16 become trapped in the filter media 11, and a quiet zone 15 where particulates 16 to be filtered out of fluid 21 can settle.

10 Fluid enters through exit holes 27 in an influent ring 26, which is supplied fluid from influent pipe 25. Fluid exits tank 30 through effluent pipes 22. Effluent pipes have a filter area 23 for preventing filter media 11 from exiting therethrough with fluid 21.

15 There is a conveyer means 40 for moving filter media 11 in a direction counter to the direction of flow of fluid 21 through tank 30, from the top of the filter zone 19 to quiet zone 15. Conveyer means 40 could comprise, for example, a plunger pump or a propeller pump, but in the
20 first embodiment of the present invention it comprises an auger 41. Conveyer means 40 includes auger 41 and a counter-direction friction duct 42 containing auger 41 (suitable means, not shown, secure duct 42 within tank 30). There is a motor 45 (preferably variable-speed) for turning
25 auger 41.

Duct 42 includes an entrance 44, a closed bottom 46, and exit holes 43 adjacent the bottom 46 of duct 42. Exit holes 43 are preferably as open as possible to prevent clogging.

30 Auger 41 includes a shaft 48 and flighting 47 attached to shaft 48.

A pump 24 pumps water from fish tank 50 to tank 30.

In operation, a sufficient quantity (such as 80-100 cubic feet when tank 30 has a volume of 120-150 cubic feet)
35 of buoyant filter media 11 (preferably polypropylene or polyethylene beads having an average diameter of approximately $3/32 - 1/8$ inch) is placed in filter

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apparatus 10 of the first embodiment of the present invention. Fluid 21 (e.g., water) to be filtered enters tank 30 via influent pipe 25, influent ring 26, and exit holes 27 in influent ring 26. Fluid 21 moves into mixing zone 18 where particulates 16 and the filter media 11 mix. Fluid 21 then moves into filter zone 19 where particulates 16 in fluid 21 become trapped in the filter media 11. After passing through filter zone 19, fluid 21 passes through the filter area 23 of effluent pipes 23 and passes out of tank 30.

While fluid 21 is passing from the influent pipe 25 through tank 30 and out of effluent pipes 23, the filter media 11 is being moved in the opposite direction by conveyer means 40. Conveyer means 40 includes an auger 41 (preferably 6" or 9" diameter Helicoid Conveyer Screw), a counter-direction friction duct 42 containing auger 41 (suitable means, not shown, secure it within tank 30), and a motor 45 (preferably variable-speed) for turning auger 41. Duct 42 includes an entrance 44 and exit holes 43 in the closed bottom 46 thereof. Auger 41 includes flighting 47 attached to a shaft 48. Conveyer means 40 pulls filter media 11 downward (upstream) from the top (downstream side) of filter zone 19 to quiet zone 15 of tank 30, where the filter media 11 and particulates 16 separate, with particulates 16 settling to the bottom of tank 30 in the quiet zone 15, and filter media 11 floats upward into the mixing zone 18. When a sufficient quantity of particulates 16 has accumulated in the conical bottom 32 of tank 30, valve 34 of waste outlet 33 is opened to allow them to exit tank 30.

Conical top 35 of tank 30 (filter media control cap) contains the filter media 11.

Pump 24 pumps water from fish tank 50 to tank 30.

Filter apparatus 110, the filter apparatus of the second embodiment of the present invention, is shown in Figs. 3 and 4. Filter apparatus 110 includes a tank 130 having a cylindrical wall 131, a conical bottom 132, and a

1 dome-shaped top 135. There is a quiet zone 115 in tank
2 130, a mixing zone 118 where particulates 16 and the filter
3 media 11 mix, and a filter zone 119 where particulates 16
4 become trapped in the filter media 11. Adjacent conical
5 bottom 132 of tank 130 is a waste outlet 133 having a valve
6 134. There are four blades 160 in quiet zone 130 to help
7 make zone 130 even quieter (i.e., less turbulent).

8 There is a conveyer means 140 for conveying filter
9 media 11 from the top of tank 130 to quiet zone 115.
10 Conveyer means 140 comprises an auger 141, a counter-
11 direction friction duct 142 containing auger 141, and a
12 motor for turning auger 41 (preferably variable-speed - not
13 shown, but it can be the same as motor 45). Duct 142
14 includes entrance vents 144 adjacent the top thereof, a
15 closed bottom 146, and exit vents 143 in the bottom
16 thereof.

17 There is a nylon bearing plate 137 adjacent the closed
18 bottom 146 of duct 142 which closes the bottom 146. There
19 is a stuffing box plate 138 adjacent the top of duct 142.
20 Threaded fittings 149 secure influent pipes 125 to
21 duct 142, while threaded fittings 139 secure pipes 125 to
22 tank 130. Influent pipes 125 may comprise schedule 40 PVC
23 or stainless steel. There are exit holes 127 in influent
24 pipes 125, with nozzles 128 in exit holes 127.

25 Auger 141 includes a shaft 148 and flighting 147.

26 There are a plurality of outer effluent pipes 122
27 (four, for example), with each pipe 122 having disposed
28 therein an inner strainer slide pipe 124. Each pipe 124
29 includes a filter area 123 which projects downwardly into
30 tank 130 out of outer effluent pipe 122.

31 Adjacent the bottom of each pipe 124 is a ball float
32 valve 151. Ball float valve 151 includes a ball retainer
33 cage 152 and a ball 153. The openings in cage 152 are
34 large enough to allow filter media 11 to pass therethrough
35 but small enough that ball 153 cannot.

In operation, a predetermined quantity of filter media
11 is placed in tank 130. Fluid 21 enters tank 130 through

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pipes 125 adjacent quiet zone 115, and is directed upward through nozzles 128 in exit holes 127 in pipes 125. Particulates 16 entrained in fluid 21 mix with filter media 11 as fluid 21 and filter media 11 move toward the top of tank 130. Filtered fluid exits tank 130 through cages 152 and pipes 122. Filter media 11 and particulates 16 that reach the top of tank 130 are drawn into duct 142 through entrance vents 144 by auger 141. Auger 141 conveys filter media 11 and particulates 16 downward through duct 142 and out of duct 142 through exit vents 143 into quiet zone 115. In quiet zone 115 filter media 11 and particulates 16 separate, with particulates 16 settling to the bottom of tank 130 and filter media 11 rising through the mixing zone 118 to filter zone 119.

15 Ball float valve 151 closes off fluid flow to effluent pipes 122 when it is desired to clean inner effluent pipe 124. When inner effluent pipe 124 is pulled upward in outer effluent pipe 122, buoyant ball 153 rises and seats against the bottom of outer effluent pipe 122, cutting off fluid flow from tank 130 into outer effluent pipe 122. Because there are a plurality of outer effluent pipes 122 and inner effluent pipes 124, it is possible to clean inner effluent pipes 124 without stopping the flow of fluid through tank 130. Inner effluent pipes 124 can be cleaned individually by pulling them upward and allowing buoyant balls 153 to rise and seat against the bottom of outer effluent pipes 122. As long as one inner effluent pipe 124 is in operation, the others can be shut down and cleaned, though it is preferable to have as many inner effluent pipes 124 as possible operating at one time to allow maximum flow rate of fluid through tank 130.

35 Because of the filter media 11 being constantly rejuvenated by conveyer means 140, and because inner effluent pipes 124 can be cleaned individually without stopping fluid flow through tank 130, tank 130 can be operated continuously, with the need to need for backwashing, as in other filters. This means that the

apparatus of the present invention can be used for considerable periods of time (for example, several months) without any down time due to backwashing.

Conical top 35 of tank 30 could be replaced with a cap which only controls the filter media 11, and which does not control fluid flow. A top for tank 30 would be positioned above such a cap. The cap could be, for example, either dome or cone shaped.

A baffle could be provided adjacent the bottom 32 of tank 30 to make quiet zone 15 even quieter.

Impurities to be filtered out with the system of the present invention could be less dense than the fluid being filtered, in which case the filter could be turned upside down and a filter media denser than the fluid could be used (e.g., if floating impurities are to be filtered out of water, the filter would be turned upside down and sand could be used as the filter media).

As can be seen, the top of the tank could be various shapes, including dome shaped or cone shaped.

Tanks 30 and 130 could be partitioned and several augers could be used to move filter media from the top (downstream end) of the tanks to the bottom (upstream end).

The present invention can be used for waste water treatment, solid removal, livestock use (for example, to clean waste water), and particle removal. Bacteria grows on bed particles.

Particles less dense than water float upward, and particles more dense settle.

All piping could be plastic or stainless steel, for example.

Tanks 30 and 130 could be insulated so that they could be used outdoors, for example.

In tank 130, effluent means other than effluent pipes 122, 124, and ball float valve 151 could be used - the primary advantage of the effluent means disclosed herein is that it is possible to clean the individual effluent means without shutting down the filtration process, thus allowing

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continuous filtration.

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The third embodiment of the present invention, filter apparatus 210, is shown in Figure 5. Filter apparatus 210 includes a tank 230 having two end walls 231, two side
5 walls 234, a curved top 233, and a V-shaped bottom 232. Internal partitions (not shown in Figure 5) divide tank 230 into four compartments 235. Each compartment 235 includes a conveyer means 140 and filter media 11, and contains the same elements and can work, for example, in the same manner
10 as apparatus 110. The plurality of individual compartments 235 are not in fluid communication with one another unless one connects the effluent of one compartment to the influent of another to make a multi-stage filter apparatus. Otherwise, the filters can filter water from various
15 sources without there being any fluid contact between the sources; this can be useful when one wishes to avoid spreading disease from tank to tank on a fish farm.

The filter apparatus of the fourth embodiment of the present invention, filter apparatus 310, includes a tank
20 330 divided by a partition 350 into a plurality of compartments 335. Each compartment 335 includes a conveyer means 140 and filter media 11 and contains the same elements and can work, for example, in the same manner as apparatus 110. Tank 330 could be, for example, the same
25 shape as tank 130.

Figures 7 and 8 show the filter apparatus
410 of the preferred embodiment of the present invention. Apparatus 410 includes a tank 430 having a cylindrical wall 431, a flat bottom 432, and an open top 435. Apparatus 410
30 also includes a conveyer means 440 including a counter-direction friction duct 442, funnel 447, influent direction-altering pipes 426, and a deflector cone 445.

Water enters tank 430 via influent pipes 425. The water is then directed downward into counter-direction
35 friction duct 442 via influent direction-altering pipes 426. The water entering duct 442 via pipes 426 causes a suction at funnel 427, drawing water, filter media 11, and

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bed, and the bed therefore becomes thicker and traps more solids and bio-flocculation (bio-floc) builds up on the bed.

When the filter media is cycled relatively slowly
5 through the conveyer means, solids and bio-floc settle out relatively easily.

When the filter media is cycled at a medium speed through the conveyer means, there is some settling of solids and bio-floc and at the same some fluidizing of the
10 bed.

When the filter media is cycled at a relatively high speed through the conveyer means, the filter bed is fluidized and the filter media is constantly rejuvenated.

The filter apparatus of the present invention settles
15 solids, causes the water to undergo a nitrification process, de-gasifies the water, and oxygenates the water.

While all embodiments of the present invention settle solids and cause the water to undergo a nitrification process, filter apparatus 410 is especially efficient in
20 de-gasifying and oxygenating the water.

To achieve better oxygenation of the water, one can add some auxiliary aeration means to the filter apparatus of the present invention. Adding auxiliary aeration means to tank 30 or tank 130 will help to keep the filter media
25 beds in those tanks from compacting. The auxiliary aeration means could inject either air or oxygen bubbles. The gas would preferably be injected above the bottom of the conveyer means.

The filter apparatus 410 of the present invention
30 provides: continuous cleaning; practically unlimited flow-through (influent, effluent), which maximizes oxygen and degasification; the overflow weir shroud adds oxygen, splash zone, shields; the overflow weir strips effluent of gas (carbon dioxide etc.); maximum use of bio-mass due to
35 cycling of total bed; even distribution of all particulates in rising bed; solids removal/capture/harvest (settleable, suspended, dissolved); minimum vessel

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pressure which promotes low head; variable speed bed cycling (static, slow, medium fast cycle); bio bed porosity continuously kept open; control of tunneling of bed by cycling continuously; maximizing of bio bed by allowing non-settleable flow to be evenly placed back in bed until bio flow mass increases to settleable proportions; bacteria air contact zone; fluidized bed zone; submerged bed zone; centrifugal pump and weir/influent injector vortex flow combination which allows maximum capacity flow to allow large applications, such as aquaculture and water treatment.

The counter direction friction duct (CDFD) cycles, separates (by friction) bio bead particulates, evenly disperses particulates in bed, aerates, provides movement, directs solids settled, bead casting (deflector zone).

Apparatus 410 allows the bio filter to operate hydraulically as well as mechanically (centrifugally pump), which is an economical energy feature.

Additional features could include: a lighted clear shroud on the outside of screens 429 to produce algae to remove nutrients from effluent water and produce algae for certain species of fish to eat; heated shroud overflow weir configurations to retain heat and heat water with Electricity/Gas/Microwave/Steam Energies; rotating shear angle rake with screen cleaning brush to prepare the upper bio bed wet beads as to shear off into open end of CDFD; insulated walls of the filter to hold heat in cold weather; heat coils in filter insulated walls to hold constant temperature.

A-1 AQUACULTURE CONTINUOUS CLEANING MULTI-FUNCTIONAL BIOFILTER

The CCMB is a hydrodynamically driven, expandable-media 11, non-clogging, self cleaning, biological reactor primarily designed for the chemical reduction of inorganic nitrogen (nitrification) in water. This water, containing inorganic nitrogen, may include, but is not limited to, aquacultural culture water, and domestic wastewater.

The reactor 510 preferably contains the following components illustrated in figure 1 for proper operation:

reactor vessel 530;

media 11;

5 media screen 529;

inlet nozzle 526;

flange 527, and;

down tube 542.

Reactor Vessel 530

10 The purpose of the reactor vessel 530 is simply to retain the water being treated and the cycling media 11. The reactor vessel 530 may be any shape so long as it can contain water and is open to the atmosphere at its top 535.

Media 11

15 Since fixed-film bacteria are utilized in this nitrifying process, a surface must be provided for colonization. In order to maximize the efficiency of the reactor 510, the surface area to volume ratio must be maximized. This is best achieved through the use of
20 granular media 11.

The granular media 11 employed in this reactor is less dense than water and expandable. Both of these characteristics are critical to the media's 11 ability to cycle properly within the reactor.

25 The media 11 provide a second function in that, as it continuously cycles through the reactor, the media 11 clean the reactor 510 and screen 529 surfaces of excess biomass.

Media Screen 529

30 Around the perimeter of the opening at the top of the reactor vessel 530 is a static screen 529. The purpose of this screen 529 is to retain the cycling media 11 as the treated water exits the reactor vessel 530. The screen 529 is usually vertical, however it may be mounted so that it makes any angle to the horizontal other than zero. The
35 media screen 529 is supported by a screen frame 590.

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Inlet Nozzle 526

Inlet water passes through an inlet nozzle 526 before entering the reactor. The inlet nozzle 526 is supported by the screen frame 590. The purpose of the nozzle 526 is to regulate the velocity of the inlet water. The velocity of the inlet water must be such that its passage through the flange 527 causes a reduction in pressure at the flange 527 opening and a lowering of the water level in the flange 527 (venturi effect). It is the force exerted by the inlet stream created by the inlet nozzle 526 which provides the driving force for the entire reactor 510.

Flange 527

The flange 527 is mounted below the top opening 535 of the reactor vessel 530 and immediately above the down tube 542. The flange 527 is supported by adjustable support rods 591 which are connected to the screen frame 590. The flange 527 provides many functions to the operation of the reactor 510. The flange 527 provides a restriction to the media 11 as the media 11 rise along the outer walls 531 of the reactor 510, resulting in a compacting of the media 11. V-notches 544 along the flange 527 perimeter allow water (recycled) from within the reactor 510 to rush into the flange 527 to fill the void created by the lowered water level created by the velocity of the inlet water. As this water rushes into the flange 527, the floating media 11 flow into the flange 527 on top of this recycled water. It is this precise combination of restriction (causing compaction of the media 11) and weir effects which forces the media 11 to rise completely out of the water before sliding (by gravity) into the flange 527.

There exists a critical venturi effect which can not be exceeded without causing such a reduction in pressure at the flange 527 that air is sucked down into the down tube 542. This critical venturi effect is controlled by positioning the flange 527, via the adjustment rods 591. Should this situation occur, the rising air bubbles will cause the rising media 11 to fluidize and expand. Thus the

media 11, without the necessary compaction, will continue to cycle, however without rising out of the water.

Down tube 542

5 The down tube 542 provides a barrier between the
expanded media 11 continuously being pushed down by the
inlet/recycled water mixture and the compressed media 11
continuously rising up in the reactor 510. The length of
the down tube 542 may be varied to produce the desired
effect. A down tube 542 which terminates above the media
10 11 level will reduce the velocity of the downward moving
media 11, as this media 11 must push through a thickness of
upward moving media 11, thus decreasing the distance that
the downward moving media 11 must travel before its
buoyancy causes a direction reversal. Conversely, a down
15 tube 542 which terminates below the media 11 level will not
restrict the velocity of downward moving media 11. The
significance of these two methods is explained in the
section on settling zone 515.

Optional Components

20 The following optional components may be incorporated
into the reactor system 510:
multi-directional effluent distribution unit (MEDU) 528;
solids capturing media;
supplemental inlets 539;
25 flow control valves;
pressure release valve;
one-way valves, and;
drain port 585.

30 Multi-directional Effluent Distribution Unit (MEDU)
528

Should the CCMFB 510 be operated outside of a fish
culture tank or if the CCMFB's effluent should need to be
directed to remote locations, a multi-directional effluent
distribution unit (MEDU) 528 can be installed adjacent to
35 the media screen 529. As water exits the reactor through
the media screen 529 it is caught in the MEDU 528 from
which it may be directed to any location by gravity and

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through pipes 522 or troughs.

Solids Capturing Media 570

The size and shape of the MEDU 528 may be varied so that it may contain any variety of solids capturing media.

- 5 This feature will allow the capture of waste-solids 16 or bacterial biomass which may escape the CCMFB 510.

Supplemental Inlets 539

- 10 While the driving force of the inlet water stream powers the continuous cycling of the media 11 within the CCMFB 510, it may be necessary to flow greater quantities of water through the reactor 510. Since increasing the flow rate through the inlet nozzle 526 would increase the venturi effect mentioned previously, supplemental inlets 539 may be installed below the media 11 level. The
15 supplemental water streams are directed such that they are horizontal and tangent to the down tube 542. These supplemental water streams cause: an insignificant reduction in reactor performance; a slight rotation of the media 11, greater compaction of the rising media 11; an
20 increase in the reactor vessel 530 pressure; an increase in the water level above the reactor vessel 530; and an increase in the distance that the media 11 travels out of the water.

Flow Control Valves

- 25 The addition of adjustable flow controlling valves to the inlet 525 and supplemental 539 lines allows the rate at which the media 11 continuously cycles to be varied. By increasing the flow rate through the supplemental inlet 529 line the media 11 compacts further and the cycling velocity
30 decreases. Additionally, the water level above the flange 527 increases and the flow rate through the inlet nozzle 526 can be increased without sucking air and "blowing" the rising media bed.

Pressure Release Valve 582

- 35 Should the inlet water to the CCMB 510 become temporarily interrupted, the media 11 (being less dense than water) may float into the inlet nozzle 526. Once flow

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is restored the media 11 may become trapped and partially clog this orifice. To avoid this problem, the water supply line 525 may be fitted with a pressure release valve immediately before entering the reactor. This valve automatically opens when flow is interrupted. As the pressure release valve opens, water flows out of the nozzle 526 thus preventing media 11 from floating into the supply line 525.

One-way Valves

Should the inlet lines 525, 539 be broken, water and media 11 may flow from the CCMB 510. The addition of one-way valves on the supply lines 525, 584 will prevent this from occurring.

Drain Ports 585

Drain ports 585 may be installed on the reactor vessel 530 to facilitate removal of water or media 11 for transport purposes. The water drain 585 is typically located at the bottom of the reactor vessel 530. Media drain(s) may be located along the side wall 531 of the reactor vessel 530, usually toward the top 535 so that the media 11 may be floated out.

The water drain port 585 located at the bottom 532 of the reactor vessel 530 may serve another function for the periodic removal of biomass or particulates 16 which accumulate on the bottom 532 of the reactor vessel 530.

PROCESS DESCRIPTION

Physical

Water

Typically, water enters the CCMB 510 through both the inlet nozzle 526 and one supplemental supply line 539. Water entering the CCMB 510 through the inlet nozzle 526 passes through the flange 527 creating a venturi effect and is mixed thoroughly with expanded media 11 and recycled water which raises its dissolved oxygen content. The force of the inlet water carries this mixture down the down tube 542 where it impinges upon a layer of media 11. The combination of this collision, together with the velocity

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reduction caused by the sudden increase in cross sectional area results in a velocity drop to nearly zero.

As soon as the inlet/recycled water mixture clears the bottom of the down tube 542 it mixes with the water entering via the supplemental supply line and begins to travel towards the top of the reactor vessel 530 where it encounters media 11 which is floating upward. The water flows faster than this compacted media 11 and thus passes through the media 11 until it reaches the top. As the water reaches the top of the reactor vessel 530, it is divided three ways.

The largest portion of the flow nearest the outer wall 531 of the reactor vessel 530 flows over the edge of the reactor vessel 530 through the screen 529 and is aerated and stripped of waste gasses (degassed).

The next largest portion of water, nearest the flange 527, flows through the v-notches 544 of the flange 527 where it rushes to fill the void created by the venturi effect of the inlet water. In the process of flowing through the v-notches 544, this water is also somewhat aerated and degassed. This water then mixes with the inlet water and falling media 11 and again completes the continuous loop.

The third and smallest portion of water is entrapped within the compressed media 11 matrix (via viscous forces) as the media 11 raises out of the water. It is at this point that the entrapped water trickles down through the media 11, providing the majority of aeration and degassing. The majority of this water flows out of the CCMB 510 through the screen 529, however some flows back down into the flange 527 and continues to cycle.

Media 11

Since no media 11 enters or leaves the CCMB 510 we will, for convenience sake, name the flange 527 as the starting point of the continuous cycle.

Fluidized expanded media 11 continuously falls into the flange 527 where it is first sucked through the flange

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this media 11 is sucked through the flange 527 via the venturi action and continues the cycle.

5 The remainder of the compressed media 11 plug is now pushed completely out of the water and above the top 535 of the reactor vessel 530 by the buoyant force of the media 11 continuously rising underneath it and the force of the rising water. As the media 11 clears the top of the reactor vessel 530 it is retained in the CCMB by the static screen 529 as the majority of the water exits through the
10 screen 529. Friction forces along the surfaces of the media 11 resist water flow and some water remains with the media 11 until gravity overcomes the skin friction of the media surfaces.

As the compressed media plug continuously rises out of
15 the water and the portion nearest the flange 527 is continuously washed into the flange 527, the media plug takes on a funnel shape with the media 11 adjacent the static screen 529 rising the greatest distance above the reactor vessel 530. The funnel shape is completed as the
20 top most layer of media 11 continuously breaks free of the matrix and falls into the flange 527 along an angle of repose distinct to the physical properties of the granular media 11. As the media 11 continuously falls into the flange 527 it is sucked through the flange 527 via the
25 venturi action and continues the cycle.

Bacteria

Autotrophic nitrifying bacteria colonize the surfaces of the media 11 within the CCMB 510. The culture type can be characterized as thin film in which the biofilm is thin
30 and always in an exponential growth phase. Any excess biomass is instantaneously sheared by the force of the influent stream or by particle to particle interactions. Sheared biomass can be settled in the settling zone 515, trapped in the solids capturing media 570, or allowed to
35 flow into the fish culture tank. Biomass which flows into the fish culture tank continues to be active and contributes to *in-situ* nitrification.

Particulate Solids 16

Particulate solids 16 which flow into the CCMB 510 may be settled in the settling zone 515 and drained via the drain port 585. Solids 16 which escape the settling zone 515 encounter the filter zone 419. These solids may continue to cycle with the media 11 until they either settle into the settling zone 515, or exit through the screen 529. Solids which exit the screen 529 may become entrapped in the supplemental solids capturing media 570 contained within the MEDU 528.

COMPARISON TO OTHER NITRIFYING BIOLOGICAL REACTORS

Plate-counts have shown that despite the turbulence caused by continuous cycling, the beads are still teaming with bacteria. The theory of turbulent diffusion says that higher turbulence means thinner, more active, biofilms, but only for cells which can remain attached in the presence of high shear forces.

Why did this not happen with rotating biological contactors (RBCs)? Higher turbulence encountered at faster RBC rotational speeds causes higher nutrient and O_2 levels. This results in more bacteria which causes the film to grow thicker than diffusion can supply the inner cells with nutrients. Those inner cells either weaken or die. This combined with shear forces causes chunks of bacteria to slough off, settle, become anaerobic, and cause problems.

What makes the CCMB bacteria different from that of the RBC? The beads are exposed to far more shear than would ever be experienced by even an experimental RBC by the jet of water which forces the beads down the center of the filter and by the colliding beads. In this aspect the filter begins to look more like a fluidized sand filter where the biofilm stays thin and active.

What makes this filter better than a fluidized sand filter? In a fluidized sand filter up-flowing water pushes the sand particles up until gravity pulls them back down, while the water to be treated simply flows straight through and out at the top. However, in the CCMB, after the water

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Figures 14 and 15 show adjustment rods 591, which are the means for adjusting the height of the counter direction

friction duct. Also shown in Figure 15 is the influent centering lock collar 592 for centering the influent pipe coming into the down tube 542. Figure 15 also illustrates well how rising media 11 are compressed in the space
5 between flange 527 and the call and rise up along the outer screen 529.

Figure 16 is a top view of influent pipes 425 and adjusting rods 591. Figure 17 shows a potential arrangement of influent pipes 526 for a large (for example,
10 375 plus gallons per minute, with 125 gallons per minute through each influent pipe 526) filter.

The filters of the present invention can also be used in a solid-collecting mode (in which case the down tube would be lifted to prevent the media 11 from cycling down therethrough). As the solids collect in the lower portion
15 of the submerged bed of media 11, back pressure begins to build and water begins to belch up over the top of the flange 527 through the duct 442. At this moment, one has a down-flow solid collecting mode. As water trickles down
20 through the beads and through the screen, solids are collected at the top of the beads. When this happens, solids will be clogging the bottom and top of the bed of media 11. At this time, the filter apparatus can be changed to a cleaning mode (normal continuous cycling mode)
25 by lowering the down tube by adjusting rods 591. The solids would then flow through the screen into the gutter and flow from pipe 522 would be directed into a waste area, bypassing the original flow destination.

Mixer apparatus available from the Denver Mining Co.
30 could be used for large applications.

The filter apparatus of the present invention could be filled with water and used to filter air. In the chemical industry, catalysts could be used.

The foregoing embodiments are presented by way of
35 example only; the scope of the present invention is to be limited only by the following claims.